

**Article Info** 

Received: 24 Jan 2018 | Revised Submission: 10 Mar 2018 | Accepted: 20 May 2018 | Available Online: 15 Jun 2018

A Review of Vapor Compression-Absorption Integrated Refrigeration Systems

Vaibhav Jain\*

## ABSTRACT

This paper provides a literature review on vapor compression-absorption integrated refrigeration systems. A number of research options are suggested by researchers to integrate vapor compression refrigeration system (VCRS) with vapor absorption refrigeration system (VARS). Each way has its own pros and cons. Present work provides a detailed review on working, parametric study, advantages and disadvantages of various configurations of vapor compression-absorption integrated refrigeration systems.

Keywords: Vapor Compression; Absorption; Integrated Refrigeration Systems.

#### **1.0 Introduction**

Vapor compression refrigeration system (VCRS) is widely used refrigeration system (about 80%) and requires a large amount of electrical energy for its operation [1]. The advancement in refrigeration sector has a major impact on energy demand which approximates to 15% of the total energy consumption in the world [2]. Many developing countries like India currently suffer from a major shortage of electricity. Moreover, 56% of the total electrical capacity is generated using coal in India [3]. Not only does it exacerbate the depletion of fossil fuel, but also results in the production of harmful gases due to the burning of fossil fuel, which causes greenhouse effect and deteriorates the environment. But, energy conservation and ecological safety are the indispensable requirement the for sustainable development of any country.

One of the alternatives to reduce the dependence on electrically powered VCRS is the use of vapor absorption refrigeration system (VARS) [4]. VARS which operate on heat energy input are the second most widely used refrigeration systems. Refrigerators which operate on other types of energy input are only used in niche applications [1]. Several researchers have studied the performance of VARS considering H<sub>2</sub>O-LiBr as a working pair. This system is generally used for the air conditioning purposes as it can maintain the evaporator temperature up to  $5^{\circ}$ C [5]. For low temperature applications i.e. below  $5^{\circ}$ C,

working pair of  $NH_3$ - $H_2O$  is used in VARS [6]. But  $NH_3$ - $H_2O$  does not form an ideal pair for the absorption system because it produces ammonia mixed with water vapor at the exit of the generator. Water in the refrigerant stream can cause operational problems in the evaporator of the system. Thus  $H_2O$ -LiBr fluid pair is suitable from the view point of solubility and boiling point requirements but it cannot be used for low temperature refrigeration [4]. Chakravarthy et al. [1] suggested the use of VCRS for low temperature refrigeration.

Engineers and scientists have been constantly engaged in inventing new technologies to provide better alternatives. The idea of combining VCRS with VARS, to innovate an integrated system was looked upon a potential alternative to conventional VCRS and VARS as it economizes the use of energy The appliance of integrated resources [7]. refrigeration system keeps the potentials of both vapor compression and absorption systems, simultaneously eliminates the demerits of both [8]. The main advantage of integrated refrigeration system is that it promises significant electrical energy saving in comparison with equivalent VCRS with small payback period [9]. This system entails the simultaneous usage of electricity and heat energy for refrigeration which can be furnished as waste energy from industrial processes, solar energy, geothermal energy, etc. Even though the space required and initial installation cost for the integrated system is

<sup>\*</sup>Department of Mechanical Engineering, Maharaja Agrasen Institute of Technology, Delhi, India (E-mail: vaibhavursaathi@gmail.com)

#### 36 International Journal of Advance Research and Innovation, Volume 6, Issue 2, Apr-Jun 2018

high but the shorter payback period (8-9 years) makes them a commercially viable option. Jain et al. [9] concluded that integrated refrigeration system are promising energy efficient and decarbonizing cooling technology in near future.

There are numerous designs on the compression-absorption integrated refrigeration systems proposed in the literature and can be broadly categorized as follows:

- 1) Vapor compression-absorption refrigeration system [10-22]
- 2) Vapor compression-absorption cascaded refrigeration system [23-39]
- Series configuration
- Parallel configuration
- 3) Vapor compression-absorption combined or hybrid refrigeration system [40-42]
- 4) Other vapor compression-absorption integrated refrigeration systems [43-48]

In present paper, an exhaustive literature survey is done to provide insight for the classification, working, thermo-economic performance aspects and comparative advantages and disadvantages of various designs of vapor compression-absorption integrated refrigeration systems.

## 2.0 Vapour Compression-Absorption Refrigeration System

The principle of working of vapor compression-absorption refrigeration system (VCARS) has been given in this section. The compressor draws refrigerant vapor from the desorber and increases its pressure to absorber pressure by consuming electrical energy in compressor as shown in Figure 1 [10]. The refrigerant vapor mixes with weak solution in the absorber and the heat generated in the absorption process is released to the atmosphere. The strong solution is throttled to the desorber pressure and sent to the desorber at low pressure and temperature. This low temperature and low pressure strong solution is deprived of refrigerant vapor by absorbing the heat from source i.e. the medium to be cooled. The refrigerant vapor generated in the desorber is sucked by the compressor and the remaining weak solution is supplied to the absorber by means of a pump. Hence, cooling and heating effects are produced in the desorber and absorber respectively.

The VCARS offers the following advantages over conventional VCRS [10].

- Non-isothermal heat exchange takes place in the absorber and desorber. Therefore, gliding temperature profile in absorber and desorber is possible which increases the theoretical COP of the cycle.
- The use of mixture allows low pressure levels in the system by changing the concentration of one component in the mixture. This allows low pressure ratio across the compressor which increases the compressor life and requires less electrical energy.
- Better capacity control is possible.
- VCARS offers the advantage of ozone friendly technology due to the use of natural working fluids like NH<sub>3</sub>-H<sub>2</sub>O and H<sub>2</sub>O-LiBr etc.

# Fig 1: Schematic Diagram of Vapor Compression-Absorption Refrigeration System [10]



A detailed simulation of 400 kW ammonia– water VCARS has been presented by Pratihar et al. [10] for water chilling application. The results showed that the COP of the system can be increased by maintaining low mass flow rate of weak solution and large relative solution heat exchanger area. Increase in the solution heat exchanger area from 10 to 30% resulted in an increase in COP by 16%. Usually VCARS are preferred over VCRS for applications where the external temperature gradients are large [11] but Ahlby et al. [12] showed that the VCARS can also be used for applications, where the external temperature gradients are small by optimizing the working conditions.Bourouis et al. [13] evaluated the performance of compressionabsorption heat pump using ternary working fluid Trifuoroethanol-Water-Tetraethylenglycol-

dimethylether for upgrading waste heat. The results showed that the ternary system is more advantageous than the binary working pair. Hulten and Berntsson [14-15] evaluated the performance of compressionabsorption heat pump using ammonia/water pair. The COP of system can be improved by allowing a higher absorber pressure (40 bar). Kim et al. [16] presented that the compression-absorption system offers many advantages over conventional vapor compression heat pumps including a large temperature glide, animproved temperature lift, a flexible operating range, and greater capacity control. Other Researchers [17-22] have also analyzed the potential of VCARS for the refrigeration purpose.

## Fig 2: Schematic Diagram of Vapor Compression-Absorption Cascaded Refrigeration System in Series Configuration [23]



# 3.0 Vapor Compression-Absorption Cascaded Refrigeration System

VCRS can be cascaded with VARS either in series or parallel [23] called vapor compressionabsorption cascaded refrigeration system (VCACRS). In the series configuration, condenser of VCRS rejects heat to the evaporator of VARS as depicted in Figure 2.

The consumption of electricity in the compressor of the VCRS is reduced as the condensation of the vapor refrigerant occurs at low temperature. The literature reviewed on series configuration is as under:

Cimsit and Ozturk [23] analysed theoretically the performance of VCACRS with H2O-LiBr and NH<sub>3</sub>-H<sub>2</sub>O as fluid pair in absorption section and R134a, R410A and NH<sub>3</sub> refrigerants in the compression section of cascaded refrigeration system. It was presented that electrical energy consumption in the cascaded refrigeration cycle was 48-51% lower than conventional VCRS. Chinnappa et al. [24] described a VCACRS consisting of a conventional R22 VCRS cascaded with a solar operated, NH<sub>3</sub>-H<sub>2</sub>O, VARS for air conditioning application. It was found to vield 49.5% saving in electrical energy consumption by the compression system.

Fernandez-Seara et al. [25] carried out the theoretical study to analyze a VCACRS from the view point of first law of thermodynamics. The system was integrated with a cogeneration system having exhaust gas temperature upto 873 K and it was found that electrical energy consumption was reduced by 133% in one of the configuration. The CO<sub>2</sub> and NH<sub>3</sub> were used as refrigerants in the compression section and NH<sub>3</sub>-H<sub>2</sub>O as the working pair in absorption section. Kairouani and Nehdi [26] theoretically studied the comparative performance of three refrigerants (R717, R22, R134a) in the compression section with NH<sub>3</sub>-H<sub>2</sub>O fluid pair in the absorption section of the VCACRS. Geothermal heat was supplied in the generator at the temperature of 335 K for a fixed evaporation temperature of 263 K. The highest performance was obtained by R717. They achieved a refrigeration effect of about 10 MW with the compressor power of 1.65 MW and reported that the same refrigeration effect could be produced by a conventional VCRS by consuming 3.6 MW of electricity which was 54% more than the combined installation consumption. Garimella et al. [27]

modelled VCACRS for naval ship application where the absorption section was powered by the exhaust heat from the on-board gas turbine power plant. An energy and economic analysis was presented by Marimon et al. [28] where a trigeneration system was integrated with an indirect cascaded refrigeration system for super market application with maximum refrigeration capacity of 100 kW. CO<sub>2</sub> was used as refrigerant in compression section whereas NH<sub>3</sub>-H<sub>2</sub>O fluid pair was used in the Several absorption section. tri-generation configurations have been studied. They all showed a payback period of less than 6 years and it was concluded that novel trigeneration system is economically feasible and environmentally viable than conventional supermarket systems. Sevfouri and Ameri[29] analysed a VCACRS in which the compressor was powered by a microturbine and the waste heat from the turbine was used to drive the absorption section. In this study, H<sub>2</sub>O-LiBr pair was considered as the working fluid in the absorption section whereas R22 was considered in compression section. A solar assisted VCACRS was studied by Wang et al. [30].

Goktun and Deha[31] investigated the effect of internal irreversibility on the performance of solar assisted VCACRS.Based on first and second law of thermodynamics, Colorado and Velazquez [32] analyzed a VCACRS with the aim of finding the best pair of working fluid. H<sub>2</sub>O-LiBr was used in the absorption section and NH<sub>3</sub>, R134a and CO<sub>2</sub> were evaluated in the compression section. The COP values estimated for R134a, NH<sub>3</sub> and CO<sub>2</sub> were 0.5852, 0.5819 and 0.5435 respectively; whereas, the exergetic efficiency of system was 0.2983, 0.2966 and 0.2685 respectively. R134a-H<sub>2</sub>O/LiBr fluid pair was reported to be a better alternative in VCACRS. In another study by Colorado and Rivera [33], comparison of the performance of two VCACRS was presented wherein single effect and double effect VARS were cascaded with conventional VCRS. The performance was better with double effect VARS since COP was improved by 36.3% using R134a-H<sub>2</sub>O/LiBr fluid pair.Cimsit et al. [34] also performed energy and exergy analyses in order to determine the best suitable working pair in the cascaded refrigeration system. The performance of H<sub>2</sub>O-LiBr and NH<sub>3</sub>-H<sub>2</sub>O fluid pairs was compared while considering R134a in the compression section. In the case of H<sub>2</sub>O-LiBr fluid pair, the COP was 27% higher and total exergy destruction rate was 20% lower as compared to  $NH_3$ - $H_2O$  fluid pair. In a study, presented by Jain et al. [35], payback period for series configuration of VCACRS was estimated to be 4.5 years. In another economic study by Jain et al. [36], it has been reported that the cascading of VCRS with VARS becomes attractive for lower rate of interest and increase life span and operational period.

Another way to cascade the VCRS with VARS is the parallel configuration, where the cooling duty is shared by both the refrigeration systems (Figure 3). The product is first cooled in the evaporator of absorption section followed by the evaporator of compression section [37]. The saving in electrical energy is obtained by reducing the cooling load on the VCRS.

# Fig 3: Schematic Diagram of Vapor Compression-Absorption Cascaded Refrigeration System in Parallel Configuration [37]



Mohammadi and Ameri [7] theoretically analysed parallel configuration of VCACRS powered by a micro gas turbine based on first and second law of thermodynamics.  $H_2O$ -LiBr fluid pair was used in absorption system whereas R22 was used in vapor compression chiller. It was concluded that the cascade configuration of system would increase the efficiency of energy usage upto 50% as compared to the equivalent VCRS.

Sun and Guo[37] set up a prototype parallel configuration of VCACRS for air conditioning

application with the cooling capacity of 589 kW where a gas engine drove directly the screw compressor in a vapor compression chiller and waste heat from the gas engine was used to operate vapor absorption system. R22 and  $H_2O$ -LiBr fluid pair were used in compression and absorption systems respectively.

Primary energy rate (*PER*) and comparative primary energy saving were used as the key parameters to evaluate energy utilization efficiency of the cascaded refrigeration system.

The *PER* of 1.81 was obtained with the prototype and it saved more than 25% of primary energy as compared to the conventional electrically driven VCRS.

Sun [38] fabricated the experimental facility and tested prototype VCACRS for central air conditioning which was also driven by a gas engine. R22 and H<sub>2</sub>O-LiBr fluid pair was used in compression and absorption systems respectively.

The experimental results showed that the refrigeration capacity of VCACRS reached 596.2 kW when the speed of gas engine was 1800 rpm. *PER* of prototype reached 1.84 at the rated conditions.

The refrigeration capacity of the set up got reduced and energy utilization ratio of the system increased with the decrease of gas engine speed. Jeong et al. [39] constructed a gas engine driven VCACRS for air conditioning application using  $H_2O$ -LiBr fluid pair in absorption section and  $NH_3$  in compression section.

The system COP at the design point was about 1.87 and, at 50% partial load operation, the performance increased by 14% because of the simultaneous manipulation of the input gas flow rate and hot water flow rate.

Jain et al. [9] presented the comparative performance study of series and parallel configurations of VCACRS based on combined energy, exergy, economic and environmental (4E) analyses.

The power consumption in the compressor of parallel and series configurations is reduced by 50% and 76.6% respectively as compared to equivalent VCRS [9].

The capital cost of parallel and series configurations is 3.1 and 3.6 times respectively more than equivalent VCRS which is the main drawback in successful implementation of VCACRS. But, the shorter payback period makes them commercially viable option [9].

# 4.0 Vapor Compression-Absorption Combined Or Hybrid Refrigeration System

A vapor compression-absorption combined or hybrid refrigeration system (VCAHRS) offers the choice of using high grade energy (electricity) or low grade energy (heat) to produce required refrigeration effect. It is capable of operating in different modes and can be utilized roundthe clock depending upon the availability of the specific energy sources, i.e. heat energy or electrical energy [40].

# Fig.4 Schematic Diagram of Vapor Compression-Absorption Combined or Hybrid Refrigeration System [41]



When the cooling capacity of the absorption system cannot meet the cooling demand of the system, the compression system works totake partial or full cooling load. The operating strategy of the combined refrigeration system ensures the absorption system to work prior to the compression system as depicted in Figure 4. Many researchers [5, 41-42] have analyzed the potential of VCAHRS.

## 5.0 Other Vapor Compression-Absorption Integrated Refrigeration Systems

In addition to above mentioned systems, there are different possible configurations to integrate VCRS with VARS. Boer et al. [43], Janghorban Esfahani et al. [44] and Meng et al. [45] integrated the VCRS and VARS in such a way that compressed vapor after superheating in the compressor is absorbed in the absorber by the weak solution coming from the generator. Anand et al. [46] used the compressor in VARS in between the generator and condenser. Han et al. [47] proposed vapor compression-absorption system which is integrated by an absorber and a rectifier. Xu et al. [48] used different concept to cascade VCRS and VARS. The refrigerant in the compression subsystem was condensed by the ambient air or water first. Then, the condensed refrigerant was supercooled by an absorption subsystem. The advantage of the consequence was that the high temperature cooling capacity provided by the absorption subsystem was upgraded to the low temperature cooling capacity of the compression subsystem.

Researchers have used different ways to integrate VCRS with VARS. Each way has its own pros and cons. The application of integrated refrigeration systems maintains the advantages of both VCRS and VARS while minimizing the limitations of both the systems. The compression system of such refrigeration system is generally operated by the shaft work of gas engine or turbine whereas the waste heat from the gas engine or turbine is used as a heat source for the generator of absorption section. By recovering the waste heat from the gas engine or turbine, the primary energy utilization efficiency of integrated system beats the equivalent VCRS. Hence, integrated refrigeration system is having high energy utilization efficiency, which not only saves the running cost but also contributes the additional environmental benefits.

#### **6.0** Conclusions

In consequence of electrical energy shortage and environmental issues related to the global warming and ozone layerdepletion attributed to the application of VCRS, the utilization of decarbonizing and energy efficient cooling technology for refrigeration purposes appears to be an appropriate alternative. Researchers have been constantly engaged in inventing new cooling technologies to provide better alternatives. Different configurations of VCRS and VARS are suggested in the literature to Economize the use of energy resources. The integrated system substantially reduces the electrical energy consumption as compared to an equivalent VCRS as it entails the simultaneous usage of electricity and heat energy for the refrigeration which can be furnished as waste heat fromindustrial processes. Hence, the operating cost of integrated refrigeration is very less as compared to equivalent VCRS. But, the main hindrance in the practical application of integrated system is their size and initial investment cost. But, shorter payback period makes them commercially viable option.

### References

- V Chakravarthy, R Shah, G Venkatarathnam. A review of refrigeration methods in the temperature range 4-300 K, Journal of Thermal Science and Engineering Applications, 3(2), 2011, 1-18.
- [2] A Arora. Energy and exergy analyses of compression, absorption, and combined cycle cooling systems (Ph.D. Thesis), Centre for Energy Studies, IIT Delhi, India, 2009.
- [3] http://www.en.wikipedia.org/wiki/Electricity \_sector\_in\_India.
- [4] CP Arora. Refrigeration and air conditioning, Tata McGraw-Hill Pub. Co., New Delhi.2000
- [5] R Ayala, C Heard, F Holland. Ammonia / lithium nitrate absorption / compression refrigeration cycle. Part I. Simulation', Applied Thermal Engineering, 17(3), 1997, 223-233.
- [6] R Best, C Heard, P Pena, H Fernandez, F Holland. Developments in geothermal Mexico-Part twentv energy in six: Experimental assessment of an ammonia/water absorption cooler operating on low enthalpy geothermal energy, Heat Recovery Systems and CHP, 10(1), 1990, 61-70.
- [7] SH Mohammadi, M Ameri. Energy and exergy comparison of a cascade air conditioning system using different cooling

- [8] strategies, International Journal of Refrigeration, 41, 2014, 14-26.
- [9] Ι С Cimsit. Ozturk, 0 Kincay. Thermoeconomic optimization of LiBr/H2O-R134a compression-absorption cascade refrigeration cycle', Applied Thermal Engineering, 76, 2015, 105-115.
- [10] V Jain, G Sachdeva, SS Kachhwaha. Energy, exergy, economic and environmental (4E) analyses based comparative performance study and optimization of vapor compressionabsorption integrated refrigeration system, Energy, 91, 2015, 816-832.
- [11] A Pratihar, S Kaushik, R Agarwal. Simulation of an ammonia-water compression-absorption refrigeration system for water chilling application', International Journal of Refrigeration, 33(7), 2010, 1386-1394.
- [12] L Ahlby, D Hodgett, R Radermacher. NH<sub>3</sub>/H<sub>2</sub>O-LiBr as working fluid for the compression/absorption cycle, International Journal of Refrigeration, 16(4), 1993, 265-273.
- [13] L Ahlby, D Hodgett, T Berntsson. Optimization study of the compression/absorption cycle, International Journal of Refrigeration, 14(1), 1991, 16-23.
- [14] M Bourouis, M Nogues, D Boer, A Coronas. Industrial heat recovery by absorption/compression heat pump using TFE-H<sub>2</sub>O-TEGDME working mixture, Applied Thermal Engineering, 20(4), 2000, 355-369.
- [15] M Hulten, T Berntsson. The compression/absorption cycle - influence of some major parameters on COP and a comparison with the compression cycle, International Journal of Refrigeration, 22(2), 1999, 91-106.

- [16] M Hulten, T Berntsson. The compression/absorption heat pump cycle conceptual design improvements and comparisons with the compression cycle, International Journal of Refrigeration, 25(4), 2002, 487-497.
- [17] J Kim, S Park, Y Baik, K Chang, H Ra, M Kim, Y Kim. Experimental study of operating characteristics of compression/absorption high-temperature hybrid heat pump using waste heat, Renewable Energy, 54, 2013, 13-19.
- [18] A Pratihar, S Kaushik, R Agarwal. Simulation of an ammonia-water compression-absorption refrigeration system for water chilling application, International Journal of Refrigeration, 33(7), 2010, 1386-1394.
- [19] A Pratihar, S Kaushik, R Agarwal. Performance evaluation of a small capacity compression–absorption refrigeration system, Applied Thermal Engineering, 42, 2012, 41-48.
- [20] P Satapathy. Exergy analysis of a compression-absorption system for heating and cooling applications, International Journal of Energy Research, 32(13), 2008, 1266-1278.
- [21] P Satapathy, M Gopal, R Arora. Studies on a compression-absorption heat pump for simultaneous cooling and heating, International Journal of Energy Research, 28(7), 2004, 567-580.
- [22] P Satapathy, M RamGopal. Experimental studies on a compression-absorption system for heating and cooling applications, International Journal of Energy Research, 32(7), 2008, 595-611.
- [23] S Tarique, M Siddiqui. Performance and economic study of the combined absorption/compression heat pump, Energy Conversion and Management, 40(6), 1999, 575-591.

#### 42 International Journal of Advance Research and Innovation, Volume 6, Issue 2, Apr-Jun 2018

- [24] C Cimsit, I Ozturk. Analysis of compression-absorption cascade refrigeration cycles, Applied Thermal Engineering, 40, 2012, 311-317.
- [25] J Chinnappa, M Crees, SS Murthy, K Srinivasan. Solar-assisted vapor compression/absorption cascaded airconditioning systems, Solar Energy, 50(5), 1993, 453-458.
- [26] J Fernandez-Seara, J Sieres, M Vazquez. Compression-absorption cascade refrigeration system, Applied Thermal Engineering, 26(5-6), 2006, 502-512.
- [27] L Kairouani, E Nehdi. Cooling performance and energy saving of a compressionabsorption refrigeration system assisted by geothermal energy, Applied Thermal Engineering, 26(2-3), 2006, 288-294.
- [28] S Garimella, A Brown, A Nagavarapu. Waste heat driven absorption/vapor compression cascade refrigeration system for megawatt scale, high-flux, lowtemperature cooling, International Journal of Refrigeration, 34(8), 2011, 1776-1785.
- [29] M Marimon, J Arias, P Lundqvist, J Bruno, A Coronas Integration of trigeneration in an indirect cascade refrigeration system in supermarkets, Energy and Buildings, 43(6), 2011, 1427-1434.
- [30] Z Seyfouri, M Ameri. Analysis of integrated compression-absorption refrigeration systems powered by a microturbine, International Journal of Refrigeration, 35(6), 2012, 1639-1646.
- [31] L Wang, A Ma, Y Tan, X Cui, H Cui. Study on Solar-Assisted Cascade Refrigeration System, Energy Procedia,16, 2012,1503-1509.
- [32] S Goktun, I Deha. The optimum performance of a solar-assisted combined absorption-vapor compression system for air

conditioning and space heating, Solar Energy, 71(3), 2001, 213-216.

- [33] D Colorado, V Velazquez. Exergy analysis of a compression-absorption cascade system for refrigeration, International Journal of Energy Research, 37(14), 2013, 1851-1865.
- [34] D Colorado, W Rivera. Performance comparison between a conventional vapor compression and compression-absorption single-stage and double-stage systems used for refrigeration, Applied Thermal Engineering, 87, 2015, 273-285.
- [35] C Cimsit, I Ozturk, M Hosoz. Second law based thermodynamic analysis of compression-absorption cascade refrigeration cycles, Journal of Thermal Science and Technology, 34(2), 2013, 9-18.
- [36] V Jain, SS Kachhwaha, G Sachdeva. Thermodynamic performance analysis of a vapor compression-absorption cascaded refrigeration system, Energy Conversion and Management, 75, 2013, 685-700.
- [37] V Jain, Gsachdeva, SS Kachhwaha. NLP model based thermoeconomic optimization of vapor compression-absorption cascaded refrigeration system, Energy Conversion and Management, 93, 2015, 49-62.
- [38] Z Sun, K Guo. Cooling performance and energy saving of a compression-absorption refrigeration system driven by a gas engine, International Journal of Energy Research, 30(13), 2006, 1109-1116.
- [39] Z Sun. Experimental investigation of integrated refrigeration system (IRS) with gas engine, compression chiller and absorption chiller, Energy, 33(3), 2008, 431-436.
- [40] J Jeong, K Saito, S Kawai. Static characteristics and efficient control of compression and absorption type hybrid air conditioning system, International Journal of Refrigeration, 34(3), 2011, 674-685.

- [41] S Xu, J Li, F Liu, F. An investigation on the absorption-compression hybrid refrigeration cycle driven by gases and power from vehicle engines, International Journal of Energy Research, 37(12), 2012, 1428-1439.
- [42] RAyala, CHeard, FHolland. Ammonia/lithium nitrate absorption/compression refrigeration cycle. Part II. Experimental, Applied Thermal Engineering, 18(8), 1998, 661-670.
- [43] J Li, S Xu. The performance of absorptioncompression hybrid refrigeration driven by waste heat and power from coach engine, Applied Thermal Engineering, 61(2), 2013, 747-755.
- [44] D Boer, M Valles, A Coronas. Performance of double effect absorption compression cycles for air-conditioning using methanol-TEGDME and TFE-TEGDME systems as working pairs, International Journal of Refrigeration, 21(7), 1998, 542-555.
- [45] IJ Esfahani, Y Kang, C Yoo. A high efficient combined multi-effect evaporationabsorption heat pump and vapor-

compression refrigeration part 1: Energy and economic modeling and analysis, Energy, 75, 2014, 312-326.

- [46] X Meng, D Zheng, J Wang,X Li. Energy saving mechanism analysis of the absorption-compression hybrid refrigeration cycle, Renewable Energy, 57, 2013, 43-50.
- [47] S Anand, A Gupta, S Tyagi. Comparative thermodynamic analysis of a hybrid refrigeration system for promotion of cleaner technologies, Journal of Thermal Analysis and Calorimetry, 117(3), 2014, 1453-1468.
- [48] W Han, L Sun, D Zheng, H Jin, S Ma, X Jing. New hybrid absorption-compression refrigeration system based on cascade use of mid-temperature waste heat, Applied Energy, 106, 2013, 383-390.
- [49] Y Xu, F Chen, Q Wang, X Han, D Li, G Chen. A novel low-temperature absorptioncompression cascade refrigeration system', Applied Thermal Engineering, 75, 2015, 504-512.